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Study of workability of fresh concrete using high range water reducer admixtures

Ayhan Şamandar^{1*} and M. V. Gökçe²

¹Düzce Vocational School, Düzce University, 81620, Turkey.

²Civil Engineering Department, Nigde University, 51100, Turkey.

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The main issue in working with fresh concrete is the workability during filling of formwork. One of the problems found in workability is occurrence of segregation depending on w/c ratio. Segregation is strongly related to w/c ratio. The fresh concrete is usually considered as a non-Newtonian fluid since it is a mixture of aggregate, cement and water. The flow behaviour of the fresh concrete, a characteristic that is strongly related to w/c ratio, plays a crucial role in the quality of high performance concretes. The aggregates in fresh concrete cause segregation in the final product depending on the flow conditions. In this study, the mechanism of segregation in such a system was theoretically investigated. The mould filling of fresh concrete was numerically investigated and aggregates were considered as Lagrange particles. Segregation was identified from trajectories of such particles. Within this framework, fresh concretes with no admixtures (MC) and those with high range water reducer admixtures (HRWRA) (MCS) were investigated. Minimum aggregate segregation in fresh concrete mixtures without HRWRA admixtures was observed to have been higher than in mixtures containing HRWRA admixture.

Key words: Fresh concrete, flow concrete, aggregate segregation, mathematical modelling, particle size distribution.

INTRODUCTION

One of the major requirements is that during moulding, fresh concrete will easily flow with no segregation to result in a highly consolidated structure. The shape of the formwork, reinforcement steel and concrete mixture parameters may prevent the fresh concrete's consolidation (Arslan et al., 2005). Especially, the lack of consolidation in the structural system may lead to insufficient durability and costly repairs due, to excessive air pocket formations. For this reason, the ACI literature (1992), offers extensive amount of documentation on various factors contributing to congestion and the means to minimize problems resulting from such congestion, including special considerations for detailing reinforcement, formwork selection, mixture proportioning and proper placing and consolidation methods (Arslan and Subasi, 2008). Self compacting concrete (SCC) is

commonly used in strengthening reinforced concrete components damaged by earthquakes. According to Takeuchi et al. (1994), self compacting concrete is also used for restricted areas, where access for placing and consolidating fresh concrete is limited as in the case of tunnel lining.

The settlement of larger aggregate grains can be detected by the presence of bleeding water. While some quantity of the resulting bleeding water is detained in the concrete, the remaining water under coarse aggregates can rise to the surface of the concrete. And this situation may cause aggregate segregation, sedimentation of cement granules, and early hydration products in the fresh concrete that is already transformed into a dense suspension. Sedimentation and bleeding are similar phenomena. The sagging of the aggregate forces the water to move upwards. The result is an inhomogenous material with larger particles at the bottom and water at the top. This has a direct implication on permeability, durability and strength of the final product. Hoshino (1988),

*Corresponding author. E-mail: ayhansamandar@duzce.edu.tr.

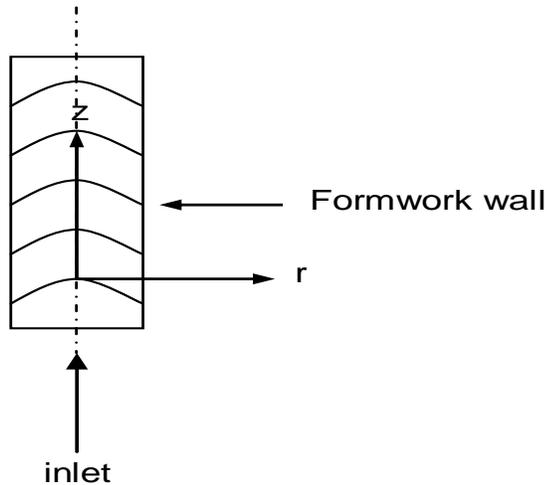


Figure 1. Schematic of test configuration (cylindrical formwork).

argues that higher w/c ratios increases the bleeding water leading to different concrete compositions at top and bottom of the structure, resulting in higher porosity.

The stability of concrete decreases with increased w/c ratio. The use of HRWRA allows improving the stability (reduction in segregation) by reducing the w/c ratio without reduction in fluidity. Khayat et al. (1993), suggested an alternative approach to enhance stability of concrete without reducing it by incorporating a viscosity-modifying admixture in combination with a HRWRA.

Khayat and Guizani (1997), indicated that regardless of w/c ratio, slump, placing height and mode of consolidation; the incorporation of a viscosity modifying admixture significantly enhanced resistance against bleeding, settlement and segregation.

According to ACI (1992), SCC is a concrete that can be cast into a mould with no excessive bleeding water, settlement and segregation having a slump of 190 mm. Wallevik (2006) investigated the relationship between Bingham parameters and slump values for flowing concrete.

The workability of flowing or SCC is defined by its rheological properties and is related to its ingredients. Ferraris (1999) defined workability either qualitatively as the ease of placement or quantitatively by rheological parameters. Tattersall's (1976) interpretation of workability is "the ability of concrete to flow in mould or formwork perhaps through congested reinforcement, the ability to be compacted to a minimum volume, perhaps the ability to perform satisfactorily in some transporting operation or forming process and may be other requirements as well". According to Tattersall (1976), the most common rheological parameters of the flow concrete, used to qualify workability, are the yield stress and plastic viscosity as defined by the Bingham equation. de Larrard et al. (1998) found in some cases that the

Herschel-Bulkley equation suited better to describe concrete flow, especially in SCC. Herschel-Bulkley equation encompasses three parameters two of which do not represent a physical entity. However, the Bingham equation is commonly employed by most researchers. The reason for this is that the parameters used in the equation are independently measurable factors. As shown by Tattersall (1976) the flow of real concrete seems to follow this equation fairly well in most cases. Recently, further research for fresh concrete rheology has been conducted both analytically and experimentally (Safawi et al., 2004; Li, 2007; Leeman and Winnefeld, 2007; Bethmont et al., 2009).

In this paper, the effectiveness of viscosity modifying admixtures to reduce aggregate segregation of flowing concrete was numerically studied. Aggregate segregation is highly important especially in terms of structural frame. The scenario is that normal concrete with different w/c ratio is filled from bottom of formwork at different inlet velocities. The fresh concrete is assumed to behave as a non-Newtonian fluid. A group of particles are introduced at the formwork inlet and segregation is studied through the trajectories of these particles. The particles are allowed to change momentum with the continuous phase. The data on the rheological properties of the fresh concrete used in this investigation to validate the proposed numerical model were extracted from results of a study made by Ferraris and de Larrard (1998).

Significance of the research

Concrete is composite material, with aggregates, cement and water as the main components. It should have a homogenous dispersion with a high capacity. Therefore, SCC should have a high stability to minimize the constructional defects. The aim of this study is to present data related to concrete mixtures to produce a stable concrete that will remain homogenous and of high compacity with minimum segregation during pumping and casting. SCC has been moulded starting from the bottom of the formwork, optimizing the stability of concrete to be used in repair of the structural components damaged by earthquakes. The findings of this research should be instrumental by predicting and designing SCC for use in restricted areas.

Problems considered

The sketch of the test configuration is shown in Figure 1. It consists of a formwork-filling system. The cylindrical formwork has a uniform internal section. The concrete enters from the bottom of the formwork and progressively rises in the formwork forming a free surface. Three different heights for the formworks were chosen as 500, 1000 and 1500 mm, and radius of the formworks was 300

Table 1. Values used in calculating viscosity of fresh concrete (Ferraris and de Larrard, 1998)*.

Mixture	Specific gravity (kg/m ³)	Water/cement ratio	Herschel-Bulkley		
			Viscosity (Pa.s)	a (Pa.s ^b)	b
MC1	2.26	0.666	161	55	1.72
MC2	2.26	0.696	146	87	1.35
MC3	2.22	0.727	76	43	1.39
MC4	2.33	0.421	114	42	1.66
MC5	2.33	0.440	106	93	1.09
MC6	2.31	0.460	56	50	1.09
MC7	2.33	0.553	156	111	1.23
MC8	2.33	0.567	140	86	1.33
MC9	2.31	0.581	134	74	1.40
MC10	2.32	0.595	111	62	1.40
MC11	2.30	0.610	89	102	0.90
MC12	2.29	0.595	122	70	1.38
MC13	2.29	0.624	176	57	1.75
MCS1	2.25	0.349	561	665	0.88
MCS2	2.32	0.361	565	506	1.07
MCS3	2.32	0.373	338	191	1.39
MCS4	2.40	0.262	2956	792	1.88
MCS5	2.39	0.271	795	269	1.73
MCS6	2.37	0.281	376	132	1.70
MCS7	2.38	0.362	476	417	1.09
MCS8	2.38	0.369	479	385	1.15
MCS9	2.38	0.376	501	430	1.10
MCS10	2.38	0.383	338	147	1.56
MCS11	2.38	0.390	370	205	1.40
MCS12	2.37	0.374	425	190	1.54
MCS13	2.40	0.388	301	87	1.83

* The MC mixtures are those without HRWRA, and MCS mixtures are those with HRWRA.

mm. For specific gravity values, the data in Table 1 were used.

MATHEMATICAL FORMULATION

A mathematical representation of the formwork filling process requires solution of the equations governing the conservation of mass and momentum along with the constitutive equation representing the slurry behavior and particle dynamics. A group of aggregate particles is introduced at the inlet of the formwork and the particles are allowed to change momentum with the continuous phase. The equations for filling a plastic formwork system can be expressed in cylindrical co-ordinates by:

Continuity equation

$$\frac{1}{r} \frac{\partial}{\partial r} (\rho r v_r) + \frac{\partial}{\partial z} (\rho v_z) = 0 \quad (1)$$

Axial momentum

$$\rho \left(\frac{\partial w}{\partial t} + v \frac{\partial w}{\partial r} + w \frac{\partial w}{\partial z} \right) = \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial w}{\partial r} \right) + \frac{\partial^2 w}{\partial z^2} \right] - \frac{\partial p}{\partial z} + \rho g_z \quad (2)$$

Radial momentum

$$\rho \left(\frac{\partial v}{\partial t} + v \frac{\partial v}{\partial r} + w \frac{\partial v}{\partial z} \right) = \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v) \right) + \frac{\partial^2 v}{\partial z^2} \right] - \frac{\partial p}{\partial r} + \rho g_r \quad (3)$$

where v and w are the radial and axial velocities respectively, p is the static pressure. de Larrard et al. (1998) suggested employing Herschel-Bulkley equation to represent the rheological properties of the fresh concrete due to its non-Newtonian behavior. This relates shear stress to shear strain rate, based on the power function:

$$\tau = \tau'_0 + a \dot{\gamma}^b \quad (4)$$

where, τ is the shear stress, γ is the shear strain rate imposed on the sample, τ_0 is the yield stress, a and b are new characteristic parameters describing the rheological behaviour of the concrete. In this case, plastic viscosity can not be calculated directly. From Ferraris et al. (2001), the yield stress is calculated by the Herchel-Bulkley equation, while the viscosity is calculated using:

$$\mu = \frac{3a}{b+2} \gamma_{max}^{b-1} \quad (5)$$

where, μ is the slope and γ_{max} is the maximum shear strain rate achieved in the test, a and b are the parameters as calculated by the Herchel-Bulkley equation. For the purpose of determining the viscosity of fresh concrete the values given in Table 1 are used.

Particles physics

The evolution of the particle position Z_p is determined from the solution of the following equation proposed by Mat et al.(1999):

$$\frac{dZ_p}{dt} = w_p \quad (6)$$

in which w_p is the particle velocity vector, obtained from the following particle momentum equation:

$$m_p \frac{dw_p}{dt} = D_p (w - w_p) + m_p b_g - V_p \nabla p \quad (7)$$

where m_p is the mass of particle, D_p is the drag function, V_p is the volume of particle, p is the pressure, w is the continuous phase velocity and b_g is the buoyancy factor, and ∇p is gradient operator.

Drag function D_p can be expressed as (Fueyo et al.,1992):

$$D_p = \frac{1}{2} \rho_p A_p C_D |\omega - \omega_p|^2 \quad (8)$$

where A_p is the particle projected area and C_D is the drag coefficient. C_D is calculated from a correlation developed by Clift et al. (1978):

$$C_D = \frac{24}{Re} (1 + 0.15 Re^{0.687}) + \frac{0.42}{1.425 \cdot 10^4 Re^{-1.16}} \quad (9)$$

where Re is a particle Reynolds number defined as:

$$Re = \frac{|w_p - w_c| d_p}{\nu_k} \quad (10)$$

where ν_k is the kinematics viscosity of the continuous phase and d_p is the particle diameter.

The buoyancy factor is given by:

$$b_f = \left(1 - \frac{\rho_c}{\rho_p} \right) \quad (11)$$

Initial boundary conditions

The formwork is initially assumed to be filled with a quiescent gas (air). The semi-solid slurry is allowed to fill the formwork at $t > 0$. Only half of the formwork is considered due to symmetry at the formwork axis. The formwork wall is assumed to be impermeable and a non-slip condition to be valid on the wall. The initial boundary conditions can be expressed mathematically as:

$$t = 0 : v = \omega = 0 \quad (12)$$

$$t > 0 \text{ at } r > 0 : \frac{\partial \omega}{\partial r} = \frac{\partial v}{\partial r} = 0 \quad (13)$$

$$\text{at } r = r_o : v = \omega = 0 \quad (14)$$

$$\text{at } z = 0 : \omega = V_{in} \quad (15)$$

Numerical method

The governing equations were solved numerically with a fully implicit, finite domain scheme embodied in the PHOENICS (Rosten and Spalding, 1986) code. Since the mold filling operation involved a free surface or the interaction of two distinct media (slurry and air) separated by sharply deformed interfaces, the discretization of the governing equation with a conventional upwind scheme usually resulted in a false numerical diffusion. A van Leer (1977) scheme was employed to resolve such property interface problem.

Due to the coupling between the transport equations governing the continuous phase and particles, a three-step solution procedure was employed. In the first step, the continuous-phase equations were solved assuming there was no particle. The next step followed the integration of particle equations using the current value of continuous phase velocity and calculation of the inter-phase sources. The continuous phase equations were solved again including the particles in the last step. This procedure was repeated until a converged solution was obtained.

A grid system of 300 mm diameter, and of variable heights was employed in all computations. This grid system and a uniform time step of 0.001 s was found to

Table 2. Parameters of concrete mixtures (Ferraris and de Larrard,1998).

Concrete mixture	Dry mixture mass (%)				Composition (kg/m ³)					w/c ratio
	Gravel	Sand	Fine sand	Cement	Gravel	Sand	Fine sand	Cement	Super plasticizer	
MC1	22.5	46.2	14.3	17.0	460	944	293	347	--	0.666
MC2	22.5	46.2	14.3	17.0	455	934	290	344	--	0.696
MC3	22.5	46.2	14.3	17.0	450	925	287	340	--	0.727
MC4	40.6	26.2	8.1	25.1	851	549	170	527	--	0.421
MC5	40.6	26.2	8.1	25.1	843	543	169	522	--	0.440
MC6	40.6	26.2	8.1	25.1	834	537	167	517	--	0.460
MC7	45.0	29.0	9.0	17.0	957	617	191	362	--	0.553
MC8	45.0	29.0	9.0	17.0	952	614	190	360	--	0.567
MC9	45.0	29.0	9.0	17.0	947	611	189	358	--	0.581
MC10	45.0	29.0	9.0	17.0	943	607	189	356	--	0.595
MC11	45.0	29.0	9.0	17.0	938	604	188	354	--	0.610
MC12	57.6	19.3	6.0	17.0	1207	405	126	356	--	0.595
MC13	57.6	19.3	6.0	17.0	1194	401	124	352	--	0.624
MSC1	21.2	43.0	12.3	23.5	468	947	271	519	12.97	0.349
MSC2	21.2	43.0	12.3	23.5	465	941	269	516	12.89	0.361
MSC3	21.2	43.0	12.3	23.5	462	935	267	513	12.81	0.373
MSC4	40.0	24.9	7.1	28.0	904	563	161	634	15.86	0.262
MSC5	40.0	24.9	7.1	28.0	899	559	160	630	15.76	0.271
MSC6	40.0	24.9	7.1	28.0	893	556	159	627	15.66	0.281
MSC7	45.0	28.0	8.0	19.0	1015	632	180	429	10.71	0.362
MSC8	45.0	28.0	8.0	19.0	1012	630	180	427	10.68	0.369
MSC9	45.0	28.0	8.0	19.0	1009	628	179	426	10.65	0.376
MSC10	45.0	28.0	8.0	19.0	1006	626	179	425	10.62	0.383
MSC11	45.0	28.0	8.0	19.0	1003	624	178	423	10.59	0.390
MSC12	57.0	18.7	5.3	19.0	1278	419	120	426	10.66	0.374
MSC13	57.0	18.7	5.3	19.0	1270	416	119	424	10.59	0.388

be sufficiently refined for a numerically accurate result. A typical calculation required approximately 5 h of CPU time on a personal computer with a Pentium III processor.

RESULTS AND DISCUSSION

Many factors are affecting the workability and stability of the concrete like the geometry of the formwork, speed of filling, the mixture composition and the rheological properties of the fresh concrete. The aggregate segregation while concrete is being placed in the formworks of 300 mm diameters and 500, 1000, and 1500 mm height was numerically investigated. The results were compared to with the rheological properties of the concrete. During the filling of the concrete into the formwork, fifty percent of the inlet area was simulated and the second half of the formwork was considered to be symmetrical. The parameters of concrete mixtures used in this study are summarized in Table 2.

The aggregate segregation varies depending on the the

concrete filling speed. In this study, the optimum filling velocity of the fresh concrete to the mould was taken as $V_{in} = 0.9$ m/s. As seen in Figure 2, Bilgil and Yeşilyurt (2002) have shown that the lower segregation is linked to the higher filling velocity. They showed that segregation declines dramatically for an inlet velocity exceeding 0.9 m/s. In industrial applications, concrete pumps discharge concrete at an average speed of 1 m/s, and this fact shows that 0.9 m/s velocity corresponds with industrial applications.

Trajectories of the representative velocity of aggregate particles in flowing concrete are shown in Figures 3 and 4. Behaviors of the aggregate during filling of concretes with different w/c ratios are given as examples in Figures 3 and 4. Since filling heights of fresh concrete of different w/c ratios are variable according to Table 2, in Figures 3 and 4, the numbers of the samples of the concretes without admixtures (MC), and with admixtures (MCS) were minimized allowing the samples not to occupy more place.

In this study, the behaviour of the particles of coarse aggregate during filling of the mould was described

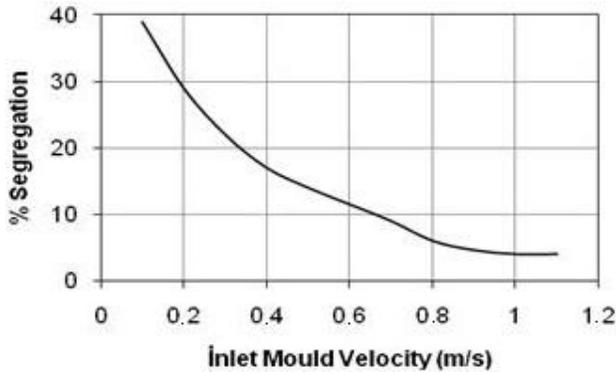


Figure 2. The percentage of aggregate segregation inlet mould velocity.

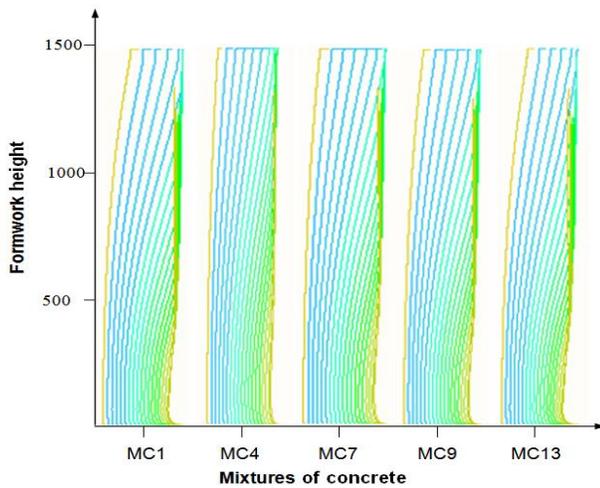


Figure 3. Trajectories of aggregate particles in formwork for different MC mixtures.

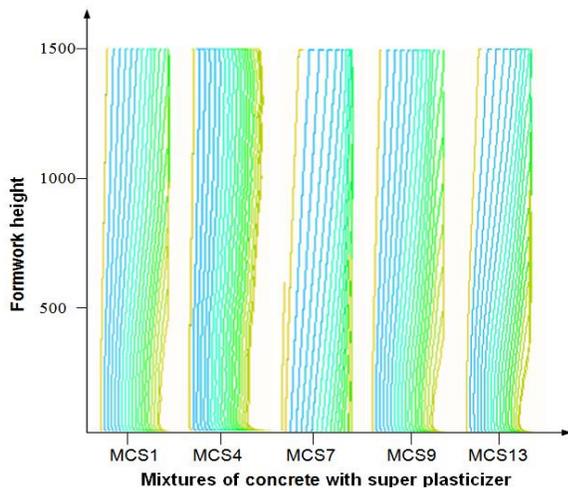


Figure 4. Trajectories of aggregate particles in formwork for different MCS mixtures.

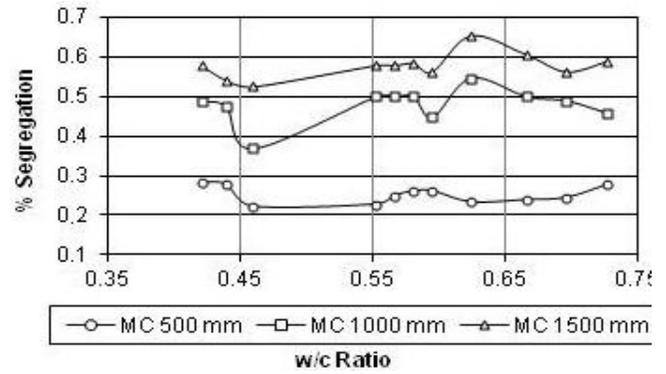


Figure 5. Effect of w/c ratios on aggregate segregation in MC mixtures.

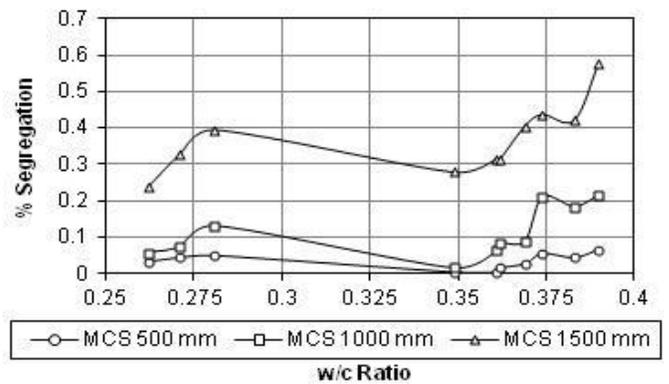


Figure 6. Effect of w/c ratios on aggregate segregation in MCS mixtures.

(Figures 3 and 4). Data on aggregate segregation of MC and MCS mixtures are prescribed in Figures 3 and 4, respectively.

Space limitations prevent describing particle behaviours of all mixtures. Moreover, similar particle behaviour in moulds of 500, 1000 and 1500 mm height allows concentrating on only the last case. Since the particle behaviours of the concrete in the moulds of heights 500, 1000 and 1500 mm were congruent, the values for 500 and 1000 mm high moulds were not given. Behaviour of particles is colour-coded as to their speed in Figures 3 and 4. Due to the effect of “boundary shear”, the movement of those particles involved are colour-coded green. At higher speed, the particles are colour-coded light blue.

Variation in aggregate segregation for MC and MCS mixtures is presented as a function of w/c ratio in Figures 5 and 6, respectively. In Figure 5, the variation of aggregate segregation for various w/c ratios was studied. h represents the height of the mould in this and subsequent figures. The fraction of segregation is defined by the following equation:

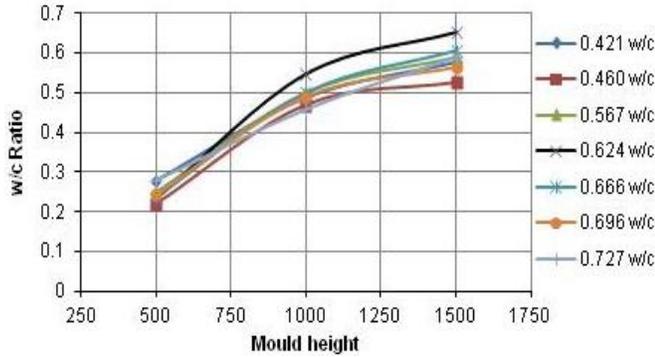


Figure 7. Aggregate segregation through mould height for different w/c ratios in MC mixtures.

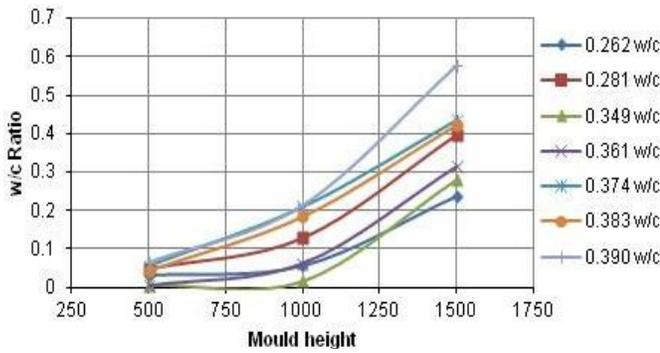


Figure 8. Aggregate segregation through mould height for different w/c ratios in MCS mixtures.

$$\eta = 1 - \frac{\sum N}{N_0} \quad (16)$$

where N_0 is the total number of particles introduced at the inlet and $\sum N$ is the predicted sum of the all particles that reached the top of the mould. On the top end of the formwork, the aggregate segregation is at its maximum value.

As seen in Figure 5, it can be seen that there is no specific w/c influence in the percentage of segregation for a given height. On the contrary, we can deduce, from Figure 6, that above a certain w/c ratio (in this case about 0.35) the segregation strongly increases.

The aggregate segregation values in the formworks of 500, 1000 and 1500 mm heights of MC mixtures were not affected dramatically by w/c ratios, and revealed a parallel segregation to each other but it was observed that segregation was affected by formwork heights. Maximum segregation was determined as 65% at w/c ratio of 0.624 and minimum segregation was determined as 53% at w/c ratio of 0.460. As indicated in Figure 6, in MCS mixtures; maximum segregation was determined to have been 58% at the mould height of 1500 mm, w/c

ratio of 0.390; and minimum segregation was determined to have been 23% at the w/c ratio of 0.262 for the same height of formwork. At the mould heights of 500 and 1000 mm, similar results were obtained. However, aggregate distribution did not present linearity in MC and MCS mixtures at different w/c ratios and the mixtures accompanied by admixtures revealed lower ratios than those accompanied by no admixtures. In MC mixtures, it has been observed that denser aggregate segregations were formed compared to MCS mixtures.

Murata and Kikukawa (1992) stated that the temperature of the mixture and viscosity of the concrete varies in considerably small values but are linear when compared to the w/c ratio. But in this study, the temperatures of the mixture and medium were neglected since the data were obtained at constant room temperature.

In Figure 7, the change in aggregate segregation with regard to mould filling height was studied for different w/c ratios of MC mixtures. As seen in the figure, aggregate segregation presents a tendency towards decreasing as the mould filling height increases. Though that decrease is not so much distinct, it might be concluded that the aggregate segregation is a function of mould height. The figure also implies that the change in w/c ratio does not have a significant effect on aggregate segregation. Thus, the conclusion that the most distinct effect on segregation is wall shear stress is achieved.

In Figure 8, the change in aggregate segregation in MCS mixtures, for different w/c ratios with regard to mould filling height was studied. As seen in the figure, aggregate segregation, to the contrary of that in MC mixtures, presents a tendency of increase as the mould filling height increases. Though this increase is not precisely linear, the conclusion that aggregate segregation in MCS mixtures is a function of mould height is achieved. However, segregation slightly increases with the increase of w/c ratio though it is not distinctly clear. Resultingly, aggregate segregation is not a function of w/c ratio, and the main factors that cause segregation are mould height and wall shear stress.

Conclusions

The degree of segregation during the formwork-filling operations of fresh concrete slurry was numerically investigated. This study, particularly assessed influence of adding a HRWRA on segregation. The degree of segregation was derived from the trajectories aggregate particles contained in the fresh concrete introduced under pressure at the bottom of the formwork. The concrete was introduced into the formwork from bottom under pressure.

The risk that the flowing concrete decomposes was observed as a function of w/c ratio and formwork height.

However, aggregate dispersions did not reveal linearity along the formwork height for different w/c ratios in MC and MCS mixtures. This situation is thought to have taken

its root from rheological properties of the concrete. Minimum degree of segregation in MC mixtures were observed to have been higher than that in MCS mixtures. Maximum degree of segregation in MC mixture was 65% for 1500 mm high formwork, while minimum segregation was 53% for the same height of formwork. For the MCS mixtures, maximum degree of segregation was 58% for 1500 mm high formwork, w/c ratio of 0.390; and minimum degree of segregation was 23% for the same height of formwork but w/c ratio of 0.262.

As the height of the formwork increases, aggregates in the MC and MCS mixtures get affected by the wall shear stress that develops on the formwork wall and this phenomenon causes segregation. Segregation shows decreasing and increasing tendency for different w/c ratios. It was observed that w/c ratios did not affect segregation especially in MC mixtures. However It was seen that aggregate segregation increased slightly as w/c ratio increased in MCS mixtures. Resultingly, it was concluded that w/c ratio did not have significant effect on segregation, and segregation is a function of formwork height.

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Nomenclature: A , particle projected area; a , b , parameters in the Herschel-Bulkley equation; C_d , drag coefficient; D , particle diameter; D , drag function; H , formwork height; M , mass; N , number of particles; P , static pressure; Re , Reynolds number; R , radial coordinate; r_o , radius of formwork; t , time; v , radial velocity; ν_k , kinematics viscosity; V_{in} , inlet velocity; W , axial velocity; Z , axial coordinate; γ , shear rate; Δ , deformation tensor; η , fractionation; μ , dynamic viscosity; ρ , density; τ , shear stress.

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